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WHAT IS CLAIMED IS:

1. A process for the preparation of crystals of zonisamide containing residual 1,2-dichloroethane of not more than 5 ppm, which comprises adding an aqueous C₂₋₄ alcohol to crystals of zonisamide containing residual 1,2-dichloroethane of more than 5 ppm, removing said 1,2-dichloroethane by azeotropic distillation, followed by collecting the precipitated crystals from the residual mixture.

2. A process for the preparation of crystals of zonisamide containing residual 1,2-dichloroethane of not more than 5 ppm, which comprises the following steps (a), (b), (c) and (d):

(a) dissolving crystals of zonisamide containing residual 1,2-dichloroethane of more than 5 ppm in an aqueous C₂₋₄ alcohol, and subjecting the mixture to azeotropic distillation;

(b) stopping the distillation after the azeotropic distillation of said 1,2-dichloroethane is completed;

(c) cooling the residual mixture obtained in the above step (b); and

(d) collecting crystals of zonisamide precipitated in the above step (c) by filtration and drying thereof.

3. A process for the preparation of crystals of

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zonisamide containing residual 1,2-dichloroethane of not more than 5 ppm, which comprises the following steps (a), (b), (c1) and (d1):

(a) dissolving crystals of zonisamide containing residual
5 1,2-dichloroethane of more than 5 ppm in an aqueous C₂₋₄ alcohol, and subjecting the mixture to azeotropic distillation;

(b) stopping the distillation after the azeotropic distillation of said 1,2-dichloroethane is completed;

10 (c1) adding the same C₂₋₄ alcohol as used in the step (a) and/or water to the residual mixture obtained in the above step (b), and dissolving the mixture with heating, and cooling thereof; and

(d1) collecting crystals of zonisamide precipitated in the
15 above step (c1) by filtration and drying thereof.

4. The process according to claim 1, wherein the aqueous C₂₋₄ alcohol is an aqueous isopropanol.

5. The process according to claim 1, wherein the aqueous C₂₋₄ alcohol is isopropanol containing water in an
20 amount of 35 to 65 % by volume.

6. The process according to claim 2, wherein the temperature at which the distillation is stopped is in the range of from 78°C to 100°C.

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